# Mineralization of pentachlorophenol by ferrioxalate-assisted solar photo-Fenton process at mild pH

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### 15 Abstract

This work reports the use of ferrioxalate complexes to assist solar photo-Fenton 16 treatment of pentachlorophenol (PCP) in aqueous medium at mild pH, which inhibits 17 the precipitation of iron hydroxides and allows working at a low iron dosage. The 18 experimental parameters were optimized by assessing the effect of initial 19 concentrations of H<sub>2</sub>O<sub>2</sub> (0-2.5 mM) and Fe(II) (2-10 mg/L), pH (3.0-9.0) and 20 iron/oxalic acid molar ratios (1:0-1:13.5) on total organic carbon (TOC) removal. 21 Ferrioxalate-assisted solar photo-Fenton achieved 97.5% mineralization in 120 min, 22 23 clearly outperforming conventional Fenton and solar photo-Fenton. The presence of photosensitive ferrioxalate complexes accounted for the enhancement, as a result of 24 Fe(II) regeneration that accelerated the hydroxyl radical ('OH) production. The time 25 26 course of H<sub>2</sub>O<sub>2</sub> and Fe(II) concentrations was evaluated under different iron/oxalic acid ratios. The five carboxylic acids determined by ion-exclusion HPLC and the 27 eight aromatic by-products identified by GC-MS allowed the proposal of a 28 29 degradation pathway that included hydroxylation, dechlorination and dimerization steps. Complete chloride ion release was achieved after 90 min of treatment. 30

*Keywords*: Ferrioxalate complexes; Mild pH; Mineralization; Pentachlorophenol;
Solar photo-Fenton

### 34 **1. Introduction**

Chlorophenols, listed as priority pollutants by most water directives worldwide 35 due to their high toxicity, are still massively employed in industrial and agricultural 36 activities (Hechmi et al., 2016; Khuzwayo and Chirwa, 2017). Pentachlorophenol 37 (PCP, C<sub>6</sub>HCl<sub>5</sub>O), the highest chlorinated phenol, is widely used as herbicide, 38 fungicide, insecticide and disinfectant, showing main applications in agriculture, 39 wood preservation and industry (Amendola et al., 2017; Tsoufis et al., 2017). 40 Although large-scale manufacture and application of PCP have been banned in 41 42 Taiwan and mainland China since 1984 and 1997, respectively, its presence in water and soil has been regularly reported in the last three decades (Shih et al., 2016). Due 43 to its long-term persistence, high toxicity and carcinogenicity, wastewater 44 45 contaminated with PCP must be conveniently treated before being discharged or reused (Cui et al., 2017). 46

The solubility of PCP, with  $pK_a = 4.75$  (He et al., 2015; Guemiza et al., 2017), is 47 highly dependent on pH, being low at pH  $< 5.0 (\le 14 \text{ mg/L})$  but very high at pH > 6.048 (> 100 mg/L) since its anionic form is predominant. As a result, it has been detected 49 in industrial wastewater of pH 9.0 at a concentration of 490 mg/L (Rahmani et al., 50 2018). Various technologies have been developed for the treatment of PCP in water, 51 52 including biodegradation (Khan et al., 2017), adsorption (Zhou et al., 2014), chemical oxidation and reduction (Shih et al., 2016), electrochemical oxidation (Niu et al., 2013) 53 and photocatalysis (Khuzwayo and Chirwa, 2017). Unfortunately, most of these 54 methods exhibit several weaknesses like long treatment times required, high energy 55

consumption, insufficient ability to ensure total removal and inefficient mineralizationthat causes the accumulation of toxic intermediates.

Nowadays, advanced oxidation processes (AOPs), including those based on 58 Fenton's reaction, ozone and light irradiation, have been proven excellent to degrade 59 highly recalcitrant organic compounds because of the action of hydroxyl radical 60 ('OH), which is the second strongest oxidant after fluorine with a high standard redox 61 potential (E = 2.80 V|SHE) (Martínez-Huitle et al., 2015). Among AOPs, Fenton's 62 reaction is recognized as a very simple way to generate 'OH. However, inefficient 63 Fe(II) regeneration usually results in the need of large amounts of such catalyst, which 64 must be carefully managed upon treatment completion (Brillas et al., 2009). The 65 addition of UV irradiation gives rise to photo-Fenton process, which can readily 66 67 regenerate Fe(II) and produce additional 'OH amounts (Eq. (1)), as well as photodecarboxylate the Fe(III) complexes generated during the oxidation of most 68 organics (Eq. (2)) (Ye et al., 2016). 69

70 
$$[Fe(OH)]^{2+} + hv \to Fe^{2+} + {}^{\bullet}OH$$
 (1)

71 
$$[Fe(OOCR)]^{2+} + hv \rightarrow Fe^{2+} + CO_2 + R^{\bullet}$$
 (2)

Nonetheless, conventional Fenton process with simple soluble salts presents two critical limitations: (i) it demands acidic conditions (pH 2.5-3.5) to maintain a high performance, which restricts the application of photo-Fenton process for wastewater treatment at large scale; and (ii) reaction (1) exhibits a quite low quantum yield for Fe(III) photoreduction ( $\Phi$ (Fe(II)) = 0.14 ± 0.04 at 313 nm), and might also be inhibited by the reduced light penetration when treating colored solutions (Pignatelloet al., 2006).

79 To overcome these disadvantages, some chelating agents such as oxalate, citrate, ethylenediamine-N,N'-disuccinic acid (EDDS), ethylenediaminetetraacetic acid 80 (EDTA) and nitrilotriacetic acid (NTA) have been investigated to upgrade the 81 conventional photo-Fenton process (Klamerth et al., 2012; Manenti et al., 2015; 82 Clarizia et al., 2017). Such compounds are able to form stable complexes with ferric 83 ions, thereby maintaining the iron soluble at less acidic pH and acting as photoactive 84 85 species that greatly enhance the performance of photo-Fenton process. Among these agents, oxalate has been shown to be preferred (Kwan and Chu, 2007). The 86 advantages of ferrioxalate-assisted photo-Fenton as compared to other systems 87 88 include (Luca et al., 2014; Souza et al., 2014; Clarizia et al., 2017): (i) the soluble ferrioxalate complex allows working at neutral pH values; (ii) this complex has a 89 higher quantum yield for Fe(II) regeneration (Eqs. (3,4)); (iii) it exhibits more intense 90 91 light absorption, with a range up to 580 nm; and (iv) additional  $H_2O_2$  production can occur from participation of dissolved oxygen (Eqs. (5-8)). The reaction network was 92 summarized as follows (Souza et al., 2014; Clarizia et al., 2017): 93

94 
$$[Fe(C_2O_4)_n]^{3-2n} + hv \rightarrow Fe^{2+} + (n-1)C_2O_4^{2-} + C_2O_4^{\circ-}$$
 (3)

95 
$$C_2 O_4^{\bullet-} + [Fe(C_2 O_4)_n]^{3-2n} \to Fe^{2+} + nC_2 O_4^{2-} + 2CO_2$$
 (4)

96 
$$C_2 O_4^{\bullet-} + O_2 \to O_2^{\bullet-} + 2CO_2$$
 (5)

97 
$$\operatorname{Fe}^{2+} + \operatorname{O}_2 \to \operatorname{Fe}^{3+} + \operatorname{O}_2^{\bullet-}$$
 (6)

98 
$$O_2^{\bullet-} + H^+ \leftrightarrow HO_2^{\bullet}$$
  $pK_a = 4.8$  (7)

$$99 \quad 2HO_2 \bullet H_2O_2 + O_2$$

(8)

Considering the high energy consumption using artificial UV light sources, 100 sunlight can be alternatively employed to operate the ferrioxalate-assisted solar 101 photo-Fenton process, which has been proven to be an efficient wastewater treatment 102 technology (Monteagudo et al., 2010; Souza et al., 2014; Expósito et al., 2018). The 103 present work investigates the mineralization and dechlorination of PCP by 104 ferrioxalate-assisted solar photo-Fenton process at mild pH with a low iron 105 concentration. The effect of main experiment parameters, such as initial 106 107 concentrations of H<sub>2</sub>O<sub>2</sub> and Fe(II), pH and iron/oxalic acid molar ratios on total organic carbon (TOC) abatement has been assessed, and the accumulation of  $H_2O_2$ , 108 Fe(II) and dissolved O<sub>2</sub> has also been determined. In addition, a schematic reaction 109 mechanism involving the iron cycle, radical reactions and PCP mineralization has 110 been proposed. A possible pathway for the degradation of PCP is presented according 111 to the identified intermediates. 112

## 113 **2. Experimental**

### 114 2.1 Chemicals

PCP was purchased from Sigma Aldrich (97% purity) and used without further purification. Hydrogen peroxide, ferrous sulfate heptahydrate and oxalic acid dihydrate were obtained from Union Chemical, Merck and Sigma Aldrich, respectively. The solution pH was adjusted with diluted NaOH or H<sub>2</sub>SO<sub>4</sub>. Other chemicals used herein were of analytical grade. Laboratory-grade deionized water from a reverse osmosis system (resistivity > 18.2 M $\Omega$  cm) was used to prepare all aqueous solutions.

122 2.2 Experimental procedures

123 The experiments were carried out in an undivided glass cell filled with 1 L of PCP solution, under constant magnetic stirring and pH monitoring (see setup in Fig. 124 S1). All the trials were performed with the initial PCP concentration fixed at 50 mg/L, 125 which is almost the solubility limit of PCP at circumneutral pH. In the dark, oxalic 126 acid was mixed with the pollutant solution and then, the Fe(II) salt was added as 127 catalyst source. The mixture was homogenized for 5 min before pH adjustment. 128 129 Finally, as the cell was exposed to sunlight, a small H<sub>2</sub>O<sub>2</sub> volume was added to initiate the photo-Fenton treatment. Samples were withdrawn at different time 130 intervals, being immediately mixed with NaOH to quench the reaction and then 131 analyzed after filtration on a 0.22 µm syringe filter. The pH was controlled along the 132 experiments to keep an almost constant value. The average UVA irradiance upon 133 exposure to sunlight was measured on a UV radiometer (SENTRY<sup>®</sup>, ST-513), placed 134 135 next to the cell, which measured within the wavelength range from 290 to 370 nm. All the trials were performed between 11 am and 2 pm on sunny days from May to June 136 2017 at Tainan (Taiwan). As can be observed in Fig. S2, during this period the 137 average UVA irradiance was around 40 W/m<sup>2</sup>. Note that, UVA irradiance showed 138 approximately 7.6 W/m<sup>2</sup> difference at 11 AM between May and June. Fortunately, it 139 is believed that such difference has insignificant influence on the performance of 140 ferrioxalate-assisted solar photo-Fenton process (Souza et al., 2014). 141

The mineralization of PCP solutions was assessed from the time course of TOC, 143 measured on a TOC analyzer (Sievers 900, GE). The residual amount of H<sub>2</sub>O<sub>2</sub> during 144 the treatment was analyzed using the titanium sulfate method (Eisenberg, 1943). The 145 Fe(II) concentration was measured using the 1,10-phenanthroline method (Tamura et 146 al., 1974). Released Cl<sup>-</sup> ions were quantified by inductively coupled plasma optical 147 emission spectrometry (Ultima 2000 ICP-OES spectrometer from Horiba Scientific). 148 Dissolved oxygen (DO) was measured on an Oxi 3210 instrument from WTW. The 149 150 carboxylic acids were determined at  $\lambda = 210$  nm by ion-exclusion HPLC using a Waters 600 LC fitted with a Bio-Rad Aminex HPX 87H, 300 mm  $\times$  7.8 mm, column 151 at 35 °C. The elution was carried out by using 4 mM H<sub>2</sub>SO<sub>4</sub> as mobile phase at 0.6 152 153 mL/min. The aromatic by-products were analyzed by gas chromatography coupled to mass spectrometry (GC-MS) using an Agilent Technologies system composed of a 154 6890N gas chromatograph and a 5975C mass spectrometer operating in EI mode at 70 155 156 eV. Around 150 mL of aqueous sample was withdrawn from the cell to extract the organic components with CH<sub>2</sub>Cl<sub>2</sub> in three times (25 mL each). The resulting organic 157 solution was dried over anhydrous Na<sub>2</sub>SO<sub>4</sub>, filtered and concentrated to less than 1 158 mL under reduced pressure to be further analyzed. The mass spectra were identified 159 with support from NIST05 MS library. 160

# 161 **3. Results and discussion**

162 *3.1. Comparative study of PCP mineralization* 

163	First, a comparative study on the mineralization of PCP from an aqueous solution
164	containing 50 mg/L (i.e., 14 mg/L TOC) at pH 5.0 by different processes was
165	conducted. As shown in Fig. 1, direct solar photolysis had no effect on TOC
166	abatement for 120 min. This agrees with the low photodegradation rate constants at
167	PCP concentrations of 0.4-2.1 mg/L, within the range of $4.9 \times 10^{-2}$ -7.1×10 <sup>-2</sup> h <sup>-1</sup> , which
168	informs about the great persistence of this pollutant in the environment (Agbo et al.,
169	2011). The PCP mineralization by conventional Fenton process with 2 mM $H_2O_2$ was
170	also very inefficient due to the low Fe(II) dosage (i.e., 5 mg/L) and the expected
171	Fe(III) precipitation at pH 5.0. When the same trial was carried out in the presence of
172	1.2 mM oxalic acid, a negligible enhancement of mineralization was achieved. Under
173	such conditions, in spite of the solubilization of Fe(III) upon chelation with oxalate,
174	the regeneration of Fe(II) to promote Fenton's reaction was quite poor. A much better
175	performance was shown by processes with sunlight irradiation. Solar photo-Fenton
176	process with 5 mg/L Fe(II) and 2 mM $H_2O_2$ yielded 21% TOC decay after 120 min.
177	Such an upgrade as compared to trials in the dark can be mainly explained by the
178	photoreduction of Fe(III)-hydroxy complexes to generate Fe(II) and 'OH (Eq. (1)),
179	along with the photodecarboxylation of Fe(III) complexes of by-products formed
180	during the degradation of PCP (Eq. (2)). TOC abatement increased up to 50% in
181	ferrioxalate-assisted solar photolysis process with 1.2 mM H <sub>2</sub> C <sub>2</sub> O <sub>4</sub> . According to Eqs.
182	(3)-(8), $O_2^{-}$ and 'OH can be generated via several chain reactions in the presence of
183	O <sub>2</sub> and hence, these two radical species may play key roles for the degradation of the
184	parent molecule and its by-products. However, the limited dissolved oxygen

concentration in the solution significantly restricted the importance of Eqs. (5) and 185 (6), which allows explaining the slower PCP removal from 30 min. The most 186 effective process to degrade PCP was ferrioxalate-assisted solar photo-Fenton, 187 yielding 97.5% TOC removal at 120 min, accompanied by the precipitation of iron 188 hydroxide. Note that, although the addition of 1.2 mM H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> accounted for 28.8 189 mg/L TOC, almost total abatement organic carbon from PCP and oxalic acid was 190 attained in the ferrioxalate-assisted solar photo-Fenton process. This positive result is 191 attributed to the high yield of 'OH formed in the presence of sufficient H<sub>2</sub>O<sub>2</sub> and 192 193 efficiently regenerated Fe(II) by Eqs. (3) and (4).

194 3.2. Effect of  $H_2O_2$  and Fe(II) dosage

The amount of added H<sub>2</sub>O<sub>2</sub> plays a relevant role in ferrioxalate-assisted solar 195 photo-Fenton process, as it is the source of 'OH upon catalyzed decomposition with 196 Fe(II). Several trials were carried out with solutions of 50 mg/L PCP with 5 mg/L 197 Fe(II) and 1.2 mM  $H_2C_2O_4$  at pH 5.0, employing different  $H_2O_2$  concentrations. As 198 199 shown in Fig. 2a, the decay of TOC after 120 min of irradiation increased from 50% to 97% when the H<sub>2</sub>O<sub>2</sub> content was increased from 0 to 1.5 mM. Further increase of 200 H<sub>2</sub>O<sub>2</sub> dosage up to 2.5 mM resulted in a quicker mineralization during the first 60 201 min, whereupon close profiles were observed until reaching the same TOC removals 202 203 at the end of the treatments. The significant acceleration using up to  $1.5 \text{ mM H}_2O_2$ was then due to the faster production of 'OH from Fenton's reaction (Soares et al., 204 205 2015). However, an excess of  $H_2O_2$  was detrimental because: (i) it acts as a radical scavenger, greatly reducing the amount of 'OH according to Eqs. (9) and (10), and (ii) 206

it accelerates its self-decomposition from Eq. (11) (Vedrenne et al., 2012; Pouran etal., 2015).

209 
$$^{\circ}OH + H_2O_2 \rightarrow HO_2^{\circ} + H_2O$$
 (9)

210 
$$HO_2^{\bullet} + {}^{\bullet}OH \to H_2O + O_2$$
 (10)

211 
$$2H_2O_2 \rightarrow 2H_2O + O_2$$
 (11)

In order to elucidate the effect of Fe(II) dosage on the mineralization ability of 212 the ferrioxalate-assisted solar photo-Fenton treatment of solutions of 50 mg/L PCP, 213 Fe(II) catalysts amounts within the range of 2-10 mg/L were added in the presence of 214 215 2.0 mM H<sub>2</sub>O<sub>2</sub> and 1.2 mM H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> at pH 5.0. The results depicted in Fig. 2b illustrate a significant enhancement of TOC abatement upon increase of Fe(II) dosage within 216 the early stage (~ 20 min). Hence, a higher catalyst concentration greatly accelerated 217 218 the decomposition of H<sub>2</sub>O<sub>2</sub>, which resulted in a larger accumulation of 'OH responsible for the mineralization. However, the final TOC removal at 120 min 219 decreased from 97.5% to 91.4% when the dosage was increased from 5 mg/L to 10 220 221 mg/L. On the one hand, an excessive addition of Fe(II) promotes partial radical scavenging according to Eq. (12) (Monteagudo et al., 2010). 222

223 
$$Fe^{2+} + {}^{\bullet}OH \to Fe^{3+} + OH^{-}$$
 (12)

Furthermore, rapid accumulation of 'OH during the initial stage is associated to a quicker decomposition of oxalate ligand and iron/oxalate complex (Eq. (13)). As the treatment proceeds, an increasing amount of Fe(III) cannot be complexed and maintained soluble and stable, which stimulates the formation of  $[Fe(OH)]^{2+}$  (Eq. (14)) and its further hydrolysis and precipitation as Fe(OH)<sub>3</sub> (Eq. (15)) (Pliego et al., 2014).

229 
$$[\operatorname{Fe}(\operatorname{C}_2\operatorname{O}_4)_n]^{3-2n} + {}^{\bullet}\operatorname{OH} \to \operatorname{Fe}^{3+} + \operatorname{Oxidized} \text{ products}$$
 (13)

230 
$$\operatorname{Fe}^{3+} + \operatorname{H}_2 0 \rightleftharpoons [\operatorname{Fe}(0\mathrm{H})]^{2+} + \mathrm{H}^+$$
 (14)

231 
$$[Fe(OH)]^{2+} + 2H_2O \leftrightarrow Fe(OH)_3 \downarrow + 2H^+$$
 (15)

In addition, a larger quantity of Fe(III) hydroxyde sludge may reduce the transparency of the solution, thus reducing the photocatalysis efficiency.

# 234 *3.3. Effect of pH and iron/oxalic acid ratio*

Since PCP is quite insoluble at low pH, supersaturated PCP solutions (i.e., 50 235 mg/L) were prepared to start the experiments at pH 5.0. After 15 min of 236 237 ferrioxalate-assisted solar photo-Fenton treatment, the pH was adjusted to a given value to investigate its effect on TOC decay. As can be seen in Fig. 2c, similar trends 238 reaching more than 95% TOC removal at 120 min were obtained at  $pH \le 6.0$  in the 239 240 presence of 5 mg/L Fe(II), 2 mM H<sub>2</sub>O<sub>2</sub> and 1.2 mM H<sub>2</sub>C<sub>2</sub>O<sub>4</sub>, which demonstrates the feasibility of working at mild pH thanks to the use of ferrioxalate complexes. In 241 contrast, at  $pH \ge 7$ , TOC remained almost constant, probably as a result of massive 242 243 iron precipitation. Indeed, pH plays a crucial role regarding the speciation of iron, oxalic acid and ferrioxalate complexes (Panias et al., 1996). Different species 244 including  $H_2C_2O_4$ ,  $HC_2O_4^-$  and  $C_2O_4^{2-}$  may coexist in aqueous medium, since oxalic 245 acid exhibits two ionization equilibria ( $pK_1 = 1.25$  and  $pK_2 = 4.27$ ). C<sub>2</sub>O<sub>4</sub><sup>2-</sup>, the 246 247 predominant species at pH > 4.27, is considered as the main source to form different ferrioxalate complexes in the presence of iron, being the complex formed by HC<sub>2</sub>O<sub>4</sub><sup>-</sup> 248 negligible at pH > 2.0 (Souza et al., 2014). The performance of ferrioxalate-assisted 249 solar photo-Fenton process highly depends on the photoactivity and stability of iron 250

complexes, whose species distribution depends on both, solution pH and iron/oxalic 251 acid ratio. Fig. S3 reveals the Fe(III) speciation diagrams as a function of pH in the 252 presence of 5 mg/L Fe(II) with different iron/oxalic acid molar ratios, as determined 253 using MATLAB. The corresponding equilibrium reactions and constants are listed in 254 Table S1. As can be seen in Fig S3 (e), which shows the speciation corresponding to 255 the case in which the same Fe(II) and oxalic acid concentrations of trials of Fig. 2c are 256 used, the predominant species are  $Fe(C_2O_4)_3^{3-}$  and  $Fe(C_2O_4)_2^{-}$  at 3.0 < pH < 7.0. The 257 former ferrioxalate complex is considered as the most stable and photoactive iron 258 complex (Faust and Zepp, 1993), being efficiently photoreduced to Fe(II) that reacts 259 with  $H_2O_2$  to generate 'OH. This is highly consistent with the profiles presented in 260 Fig. 2c, evidencing an outstanding performance and negligible difference of TOC 261 262 decays when pH varied from 3.0 to 6.0. Conversely, only 3.7% mineralization was achieved once the pH of the PCP solution was adjusted to 7.0, which can be 263 accounted for by: (i) the preferential precipitation of Fe(III) over ferrioxalate 264 265 formation (Fig. S3e), (ii) the gradual photodecarboxylation of ferrioxalate complexes, which accelerates the formation of Fe(OH)<sub>3(s)</sub>, and (iii) the enhanced transformation 266 of 'OH into  $O_2$ '- at high pH. 267

Several experiments were performed at pH 5.0 to evaluate the effect of the iron/oxalic acid ratio. As shown in Fig. 2d, almost complete TOC removal was obtained at molar ratios of 1:6, 1:10 and 1:13.5, whereas only 21.4% mineralization was achieved without the addition of oxalic acid. In the absence of oxalate anion, the predominant Fe(III) species at pH 5.0 is  $[Fe(OH)_2]^+$  (Fig. S3a), which is much less

photoactive than [Fe(OH)]<sup>2+</sup> that is typically formed in conventional Fenton process 273 at pH ~ 3.0 (Eq. (1)). Using the 1:3 iron/oxalic acid ratio,  $Fe(C_2O_4)_3^{3-}$  (56.0%) and 274  $Fe(C_2O_4)_2^-$  (43.1%) account for the largest proportion of Fe(III) species at pH 5.0 275 (Fig. S3b). The higher photoactivity of these complexes enhances the regeneration of 276 Fe(II), yielding a greater mineralization as compared to the trial with 1:0 ratio (Fig. 277 2d). Increasing the iron/oxalic acid ratio to 1:6 (Fig. S3c), the molar fraction of the 278 very photoactive  $Fe(C_2O_4)_3^{3-}$  complex increases to 89.9%, with  $Fe(C_2O_4)_2^{-1}$ 279 decreasing to 10.1% at pH 5.0, which justifies the faster and almost complete TOC 280 decay. The abatement was slightly decelerated at ratios of 1:10 and 1:13.5 (Fig. 2d), 281 despite the fact that the  $Fe(C_2O_4)_3^{3-}$  species accounted for more than 95% of Fe(III). 282 because of the significant increase of initial TOC in solution from oxalic acid that 283 competed with PCP to react with 'OH. 284

It can then be concluded that the optimum performance of the ferrioxalate-assisted solar photo-Fenton process takes place at pH 5.0, with an iron/oxalic acid molar ratio of 1:6.

288 3.4. Evolution of  $H_2O_2$ , Fe(II) and dissolved  $O_2$ 

The evolution of  $H_2O_2$  and Fe(II) along the ferrioxalate-assisted solar photo-Fenton treatments collected in Fig. 2d is depicted in Fig. 3a and b, respectively. As shown in Fig. 3a, 40% consumption of  $H_2O_2$  was achieved after 120 min in the absence of oxalic acid, whereas it reached more than 93% in only 60 min at all iron/oxalic acid ratios, thus confirming the efficient Fe(II) regeneration upon photoreduction of the ferrioxalate complexes. More in detail, rising the molar ratio

from 1:3 to 1:6 accelerated the decomposition of  $H_2O_2$ , but further increase of oxalic 295 acid content slowed down the H<sub>2</sub>O<sub>2</sub> disappearance. In fact, the H<sub>2</sub>O<sub>2</sub> concentration 296 measured at 2 and 5 min using a molar ratio of 1:13.5 was even higher than that at 297 time zero, which can be attributed to the additional generation of  $H_2O_2$  from the 298 reaction sequence given by Eqs. (3)-(8). As can be observed, DO plays a major role in 299 the formation of H<sub>2</sub>O<sub>2</sub> and hence, its evolution with treatment time was evaluated in 300 different cases. As depicted in Fig.4, the concentration of oxygen dissolved in the 301 PCP solution decreased considerably in ferrioxalate-assisted solar photo-Fenton and 302 303 solar photolysis processes, whereas it remained stable in conventional Fenton and solar photo-Fenton, which verifies the key role of DO in the aforementioned reactions 304 to form  $H_2O_2$ . This means that this additional amount of  $H_2O_2$  is able to react with 305 Fe(II) to generate 'OH, which combined with other radical species ( $C_2O_4$ '-,  $CO_2$ '- and 306  $O_2$  ) is responsible for the greater TOC abatement in ferrioxalate-assisted solar 307 processes (Fig. 1). Note that the DO concentration in both ferrioxalate systems tended 308 309 to increased again from 30 min, which can be explained by the quick chemical and photochemical decomposition of ferrioxalate complexes, especially in solar 310 photo-Fenton process (Fig. 1). 311

On the other hand, Fig. 3b reveals the evolution of Fe(II) at different iron/oxalic acid ratios. The catalyst concentration decreased to less than 1 mg/L in only 2 min in the absence of oxalate because of the quick consumption by  $H_2O_2$ . The resulting Fe(III) ion was pre-eminently in a poorly photoactive form at pH 5.0 ([Fe(OH)<sub>2</sub>]<sup>+</sup>, see Fig. S3a), thus being difficult to regenerate Fe(II). The decrease in Fe(II)

concentration was greatly decelerated upon increase of oxalic acid content, which 317 confirms the very efficient photoreduction of ferrioxalate complexes. Nevertheless, 318 owing to oxalic acid decomposition, the generated Fe(III) tended to precipitate at pH 319 5.0, eventually causing the decrease of Fe(II) concentration. Theoretically, all iron 320 should be complexed at iron/oxalic acid molar ratios higher than 1:3 (Souza et al., 321 2014), but the continuous photodecarboxylation and decomposition of ferrioxalate 322 complexes by 'OH could cause the partial precipitation of iron. However, the use of a 323 large amount of oxalic acid ensures the ion stabilization by formation of ferrioxalate 324 325 complexes, especially at pH higher than 3.1. As can be seen in Fig. 3b, the concentration of Fe(II) kept the highest value (i.e., 5 mg/L) for 20 min at an 326 iron/oxalic acid molar ratio of 1:13.5, which is very positive to promote Fenton's 327 328 reaction. Nonetheless, an excessively high amount of oxalic acid increases the operation costs, causes the competition with PCP to react with 'OH and results in a 329 higher initial TOC and thus, the iron/oxalic acid ratio should be carefully considered 330 331 for real applications.

332 *3.5. Possible reaction mechanism of ferrioxalate-assisted solar photo-Fenton process* 

Based on all previous results, a reaction mechanism for the ferrioxalate-assisted solar photo-Fenton treatment of PCP is proposed in Fig. 5.  $Fe^{3+}$  can be complexed by oxalate, and the efficient photoreduction of the resulting Fe(III) complexes eventually yields Fe(II), either as free Fe<sup>2+</sup> or complexed with oxalate, which readily reacts with H<sub>2</sub>O<sub>2</sub> to generate 'OH and Fe(III) in a closed loop. However, owing to the progressive decomposition of ferrioxalate complexes, the excess of Fe(III) tends to precipitate as Fe(OH)<sub>3(s)</sub> at pH higher than 3.1. In the presence of O<sub>2</sub>, additional amounts of H<sub>2</sub>O<sub>2</sub> and concomitant radical species (C<sub>2</sub>O<sub>4</sub><sup>--</sup>, CO<sub>2</sub><sup>--</sup>, HO<sub>2</sub><sup>-</sup> and O<sub>2</sub><sup>--</sup>) can be generated according to a series of radical reactions, although their oxidization ability is much weaker than that of 'OH. Therefore, the degradation and mineralization of PCP can be pre-eminently explained in terms of reactions with 'OH, as in the case if classical Fenton's reaction.

# 345 *3.6. Identification of degradation by-products*

In surface water and sediments, the toxicity of PCP has been evidenced at 346 concentrations greater than 3 mg/L (Stepanova et al., 2000). Some intermediates 347 generated during the degradation of this target pollutant, like 3,4,5-trichlorophenol, 348 are known to be even more toxic, as the toxicity is related to the number of chlorine 349 atoms and their position (Lin et al., 2018). Therefore, the release of Cl<sup>-</sup> and the 350 generation of PCP reaction by-products have been investigated. Fig. 6a reveals the 351 evolution of Cl<sup>-</sup> ion with irradiation time during the ferrioxalate-assisted solar 352 photo-Fenton treatment of 50 mg/L PCP with 5 mg/L Fe(II), 2 mM H<sub>2</sub>O<sub>2</sub> and 1.2 mM 353 H<sub>2</sub>C<sub>2</sub>O<sub>4</sub>. As can be seen, the degradation of PCP was accompanied by a continuous 354 release of Cl<sup>-</sup>, whose concentration increased with over time up to attain 33.5 mg/L 355 (i.e., 100% release) at 90 min, thus informing about the excellent dechlorination 356 performance and the total removal of organochlorine intermediates generated during 357 the degradation of PCP in this process. Fig. 6b reveals the evolution of five carboxylic 358 acids like oxalacetic, malonic, succinic, formic and acetic resulting from the cleavage 359 of the aromatic rings. The maximum concentration of succinic acid was 5.9 mg/L at 360

30 min, whereas lower contents of the other acids were accumulated, reaching maximum values of 2.1, 1.4, 0.9 and 0.7 mg/L for malonic, oxalacetic, formic and acetic acids at 20, 30, 45 and 45 min, respectively. The accumulation of these carboxylic acids entails the occurrence of competing Fe(III)-carboxylate complexes, which efficiently enhanced the Fe(II) regeneration via Eq. (2). Moreover, all the acids disappeared in 90-120 min, confirming the almost total mineralization achieved by ferrioxalate-assisted solar photo-Fenton process.

The main transformation products (TPs) identified by GC-MS analysis included 368 four monobenzenic and four polycyclic molecules. As summarized in Table S2, these 369 corresponded tetrachlorophenol (TeCP), trichlorophenol (TriCP), 370 to trichlorohydroquinone (TrCHQ), tetrachlorohydroquinone 371 (TeCHQ), 372 hexachlorodibenzofuran (HCDF), pentachlorodibenzo-p-dioxin (PCDD), hexachlorodibenzo-p-dioxin (HCDD) and octachlorodibenzo-p-dioxin (OCDD). The 373 cleavage of C-Cl bonds yielded lower chlorinated structures like TeCP and TriCP 374 375 (Liu et al., 2004). The subsequent attack of 'OH onto their aromatic rings resulted in two hydroxylated TPs (TeCHQ and TrCHQ). Alternatively, the direct attack of 'OH 376 on C-Cl bonds of PCP can give rise to TeCHQ, which may be further dechlorinated. 377 On the other hand, several dimeric structures were identified. Since PCP mainly exists 378 as anionic form (PCP<sup>-</sup>) at pH > 4.7, hydroxylation of PCP<sup>-</sup> leads to the generation of 379 pentachlorophenoxy radical (PCP'). Then, the coupling reaction between two PCP' 380 species or PCP' and PCP<sup>-</sup> may yield OCDD and HCDF, respectively, with chloride 381 release (Fukushima and Tatsumi, 2001). Further dechlorination of OCDD caused the 382

formation of lower chlorinated derivatives like HCDD and PCDD. The degradation
routes of PCP, which are depicted in Fig. 7, on the basis of the identified by-products,
involve three paths: dechlorination, hydroxylation and dimerization.

# 386 **4. Conclusions**

Promising results were obtained for the mineralization of PCP at near-neutral pH 387 using a low iron concentration by the ferrioxalate-assisted solar photo-Fenton process. 388 More than 95% TOC abatement were achieved in 120 min. The optimized operation 389 parameters were: 5 mg/L Fe(II), 1.5 mM H<sub>2</sub>O<sub>2</sub>, pH 5.0 and iron/oxalic acid molar 390 ratio of 1:6. The presence of oxalic acid greatly enhances the performance of solar 391 photo-Fenton process due to various reasons: (i) the ferrioxalate complex ensures the 392 iron solubility at mild pH; (ii) the Fe(III) complexes with oxalate are highly 393 394 photoactive, thus allowing the continuous Fe(II) regeneration; and (iii) additional amounts of H<sub>2</sub>O<sub>2</sub> and radical species are generated with the involvement of O<sub>2</sub>. It was 395 shown that pH and iron/oxalic acid molar ratio play crucial roles on the Fe(III) 396 speciation in aqueous medium, greatly influencing the performance of the degradation 397 process. At pH 3.0-7.0 and iron/oxalic acid ratio higher than 1:3, all the iron is 398 complexed with oxalate, whereas the excess of oxalate ion remains in solution and 399 ensures the continuous formation of ferrioxalate complexes that impedes the iron 400 precipitation. The mineralization of PCP involves dechlorination, hydroxylation and 401

decarboxylation steps, as well as the formation of some dimers that can be graduallydegraded by 'OH and other radicals.

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