# Feasibility of two low-cost organic substrates for inducing denitrification in artificial recharge ponds: Batch and flow-through experiments

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# FEASIBILITY OF TWO LOW-COST ORGANIC SUBSTRATES FOR INDUCING DENITRIFICATION IN ARTIFICIAL RECHARGE PONDS: BATCH AND FLOW-THROUGH EXPERIMENTS

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### 8 Keywords

9 Denitrification, permeable reactive barrier, monitored artificial recharge, organic10 substrate, flow-through experiments, semi-arid region.

### 11 **1. Introduction**

12 Nitrate (NO<sub>3</sub><sup>-</sup>) contamination of groundwater usually originates from anthropogenic 13 sources (mainly intensive application of fertilisers and animal manure), and is a major 14 environmental problem that affects several regions of the world (Spalding and Exner, 15 1993). It is not unusual for groundwater NO<sub>3</sub><sup>-</sup> concentrations to exceed the nominal limit 16 of 50 mg L<sup>-1</sup> for drinking water set by the 98/83/EC European Union Council Directive. 17 High  $NO_{3}$  ingestion can cause methemoglobinaemia in infants and young children 18 (Magee and Barnes, 1956) and may also promote stomach cancer. Although  $NO_3^{-1}$ contamination of aquifers is a serious environmental and health issue, natural 19 20 denitrification can occur, reducing pollution levels and diminishing the severity of the 21 problem. This process is considered to be the most important reaction that attenuates 22  $NO_3$  in groundwater (Knowles, 1982). Denitrification may be defined as the dissimilatory 23 microbial reduction of  $NO_3^{-1}$  to nitrogen gas (N<sub>2</sub>) through several intermediate steps (Eq. 24 1).

25

$$NO_3^- \to NO_2^- \to NO \to N_2O \to N_2$$
 (Eq.1)

26 Denitrification takes place under anaerobic conditions where bacteria use  $NO_3^-$  as an 27 oxidant for different materials such as organic matter, sulphides and iron minerals. 1 Denitrification can proceed by the action of heterotrophic or autotrophic bacteria, which 2 oxidise organic or inorganic substrates, respectively (simplified Eq. 2, 3). In both cases, 3  $NO_3^{-1}$  is first transformed into nitrite ( $NO_2^{-1}$ ), which is actually more toxic than  $NO_3^{-1}$  (DeBeer 4 et al., 1997), with a maximum concentration in drinking water of 0.46 mg L<sup>-1</sup> (Directive 5 98/83/CE). Through successive steps,  $NO_2$  is transformed into nitric oxide (NO), which 6 can further be reduced to nitrous oxide  $(N_2O)$ ; both species are considered greenhouse 7 gases. Finally,  $N_2O$  is converted to harmless  $N_2$ .

$$5CH_2O + 4NO_3^- + 4H^+ \rightarrow 2N_2 + 5CO_2 + 7H_2O$$
 (Eq.2)

9

$$5\text{FeS}_2 + 14\text{NO}_3^- + 4\text{H}^+ \rightarrow 7\text{N}_2 + 10\text{SO}_4^{2-} + 5\text{Fe}^{2+} + 2\text{H}_2\text{O}$$
 (Eq.3)

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10 Under anaerobic conditions, nitrate may also be reduced to ammonium (NH<sub>4</sub><sup>+</sup>) by a 11 process known as dissimilatory NO<sub>3</sub><sup>-</sup> reduction to NH<sub>4</sub><sup>+</sup> (DNRA or ammonification). DNRA 12 is induced by fermentative bacteria, reducing  $NO_3^{-1}$  to  $NO_2^{-1}$  before a final reduction to 13  $NH_4^+$  (Tiedje et al., 1982).

14 When anoxic or hypoxic conditions are guaranteed, the main limitation of natural 15 attenuation of NO3- is the lack or limited availability of electron donors (Knowles, 1982). 16 Furthermore, the presence of inorganic electron donors, such pyrite, is not abundant. 17 Thus, both autotrophic and heterotrophic denitrification processes are usually limited. 18 For this reason, the most common strategy to remediate  $NO_3^{-1}$  contamination from point 19 source discharges has been the addition of an external electron donor into the system in 20 order to enhance the capacity of indigenous denitrifying biomass to reduce NO3<sup>-</sup> into 21 dinitrogen gas (Leverenz, et al., 2010; Vidal-Gavilan, et al., 2013). For economical, 22 practical and environmental reasons, an organic carbon source is the most common 23 external electron donor added to the system. Organic carbon can be incorporated into 24 the aquifer via active systems such as injection wells (e.g. Vidal-Gavilan et al., 2013) or 25 passive systems such as permeable reactive barriers, PRBs (Gibert et al., 2008; 26 Robertson et al., 2008).

27 In arid and semi-arid regions, managed aquifer recharge (MAR) is a widely used 28 technique to increase water supplies. Infiltration and artificial recharge are achieved by

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1 ponding or flowing water on the soil surface with basins, furrows, ditches or ponds 2 (Bouwer, 2002). Artificial recharge ponds (ARP) require excavation of permeable terrain 3 close to the water source (river channel, effluent from a water treatment plant (WTP), 4 etc.). A decantation pond is often included in these systems to improve water quality 5 through deposition of suspended solids. Additionally, in order to improve the quality of 6 both recharged and groundwater, the infiltration ponds can be coupled with a PRB, e.g. 7 an organic reactive layer at the bottom of the pond. The release of organic carbon into 8 the system is expected to enhance endogenous microbiology activity, improving the 9 natural attenuation rate of some target pollutants.

10 A good example of ARP coupled with PRB is located in Sant Vicenc dels Horts 11 (Barcelona, Spain), where the aguifer is recharged by Llobregat River water. Several 12 studies have shown that the organic reactive layer in this ARP has improved elimination 13 of some organic contaminants (Valhondo et al., 2014). One of the key design parameters 14 in ARP-PRB facilities is the type of material in the reactive layer. This should be effective, 15 economic and easily available. Furthermore, it must be adapted to the socioeconomic 16 circumstances of each country. In several source water used for MAR purposes, such 17 as treated wastewater, the presence of not only NO<sub>3</sub>, but also NH<sub>4</sub><sup>+</sup>, N-organic 18 compounds and other organic micropollutants, might affect the suitability of these 19 sources for using as recharge water (Miller et al., 2006; Díaz-Cruz and Barceló, 2008; 20 Kuster et al., 2010; Maeng et al., 2011). The main organic N-containing compounds 21 present in effluents of water treatment plants are amino acids, 22 ethylenediaminetetraacetic acid (EDTA), disinfection by-products, humic substances, 23 pharmaceuticals and pesticides (Pehlivanoglu-Mantas and Sedlak, 2008; Westgate and 24 Park, 2010). Therefore, MAR might significantly lower the concentration of these 25 contaminants present in the source water (Bekele et al., 2011). For sustainable 26 groundwater management, the attenuation and fate of these compounds in groundwater 27 environments during MAR must be evaluated for each specific recharge site.

28 In the framework of the project entitled "Water harvesting and Agricultural techniques in

1 Dry lands: an Integrated and Sustainable model in Maghreb Regions" (WADIS-MAR, 2 www.wadismar.eu) a MAR system consisting of ARP with an organic reactive layer will 3 be installed in the Maghreb region (in the watersheds of Oued Biskra, Algeria). The area 4 is characterized by poor soil development, low organic matter content, water scarcity, 5 increasing water demand, overexploitation of groundwater resources and high exposure 6 to nitrate contamination. In this area, recharge is mainly due to short, heavy floods 7 caused by erratic and intense short-term rainfall events (Ghiglieri et al., 2014). Before 8 implementing the ARP in the Maghreb region, laboratory feasibility tests were carried out 9 to select the best viable substrate for the reactive layer and to evaluate its capacity to 10 remove  $NO_3^{-}$ . Several organic substrates, such as compost and softwood, had 11 previously been evaluated for their use in denitrification PRBs (Gibert et al., 2008). In 12 this study, we sought to identify low-cost, easily available and easily handled organic 13 substrates with the capacity to rapidly enhance denitrification in reactive layers in ARPs 14 located in arid and semi-arid regions, where groundwater recharge periods are typically 15 short. Bearing the above criteria in mind, we selected palm tree leaves and compost, the 16 former because palm trees are typical flora in arid North African regions and the latter to 17 serve for comparison with ARPs in moderate to humid regions such as Sant Vicenç dels 18 Horts.

19 Isotopic studies coupled with chemical data are an effective tool to identify and describe 20 denitrification (Aravena and Robertson, 1998). Furthermore, multi-isotopic studies of the 21 solutes involved in the reactions, such as the  $\delta^{13}$ C of dissolved inorganic carbon and the 22  $\delta^{34}$ S and  $\delta^{18}$ O of dissolved sulphate, can help determine whether denitrification is 23 promoted by heterotrophic or autotrophic bacteria and identify the existence of 24 secondary processes such as SO<sub>4</sub><sup>2-</sup> reduction (Mariotti et al., 1988).

The major goal of this study was therefore to assess the denitrification capacity of two substrates for their potential use in ARPs. To this end, laboratory batch and column experiments were performed. The possible adverse effects, such as NO<sub>2</sub><sup>-</sup> accumulation, NH<sub>4</sub><sup>+</sup> formation and sulphate reduction, were also considered and characterised using

isotopic and modelling tools. The second goal of this study was to obtain the nitrogen
and oxygen isotope fractionations associated with the studied degradation processes to
evaluate their potential use as a tool for assessing the efficiency of future enhanced
denitrification activities at field scale.

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### 2. Experimental set-up and methods

### 6 2.1. Experimental set-up

Batch and flow-through experiments were performed with the two materials tested, commercial compost from a composting plant located in Moià (Catalonia, NE Spain) and palm tree leaves from the Maghreb region (the watersheds of Oued Biskra in Algeria). Both substrates consisted of irregular pieces of organic material between 0.3 and 2 cm in size and were used without any specific pre-treatment. The amount of N and C (%) as well as the  $\delta^{15}N$  (‰) and  $\delta^{13}C$  (‰) of both substrates was characterised (Table 1).

13 The groundwater used in all the experiments was from the Llobregat aquifer. This was 14 chosen because it is chemically comparable (Soler et al. 2016) to the watersheds of 15 Oued Biskra in Algeria groundwater and it significantly facilitated and reduced the cost 16 of the experiment. All the experiments were performed in a glove box with an argon 17 (batch experiments) or nitrogen (flow-though) atmosphere to avoid the presence of  $O_2$ . 18 Experimental oxygen partial pressure in the glove box was maintained between 0.1% 19 and 0.3% O<sub>2</sub>, and was continuously monitored by an oxygen partial pressure detector 20 (Sensotran, Gasvisor 6) with an accuracy of ±0.1% O<sub>2</sub>.

Four types of batch experiment were performed in sterilised 500 mL glass bottles. Groundwater, spiked with NaNO<sub>3</sub> in varying amounts, was added to the glass bottles (Table 2). Commercial compost batch (CCB) and palm tree leaves batch (PTB) experiments were run in triplicate using the selected material and groundwater spiked with 0.80 mM of NO<sub>3</sub><sup>-</sup> previously purged with N<sub>2</sub> for 15 min. A 'sterilised control' experiment (SCB) was carried out adding autoclaved material (palm tree leaves) to autoclaved groundwater which had been previously degassed. In addition, an 'absence

1 control' experiment (ACB) was carried out using only degassed groundwater. Batch 2 experiments with palm tree leaves lasted for 24 hours, whereas those with commercial 3 compost lasted 11 days. In the case of the experiments with compost, bottles were 4 manually shaken once a day while in the case of the experiments with palm tree leaves, 5 bottles were shaken before each sampling event. Aqueous samples (5 mL) were 6 periodically collected using sterile syringes. The number of samples was limited to 7 maintain the solution: solid material ratio at 90% of initial value.

8 The two flow-through experiments were carried out using glass cylindrical columns (35 9 cm high, 9 cm inner diameter) (Supplementary material, Figure S1). The commercial 10 compost column (CCC) was filled with 1.24 kg of compost mixed with 3.34 kg of clean 11 silica sand (Panreac®) to increase permeability and prevent flotation of the reactive 12 material. The palm tree column (PTC) was filled with 134 g of palm tree leaves mixed 13 with 3.36 kg of clean silica sand. Thus, total organic C was 40.6 and 18.2 g kg<sup>-1</sup> for CCC 14 and PTC experiments, respectively. In both experiments, the bottom of the column was 15 filled with silica balls (2 mm  $\emptyset$ ) to prevent sediment clogging the outlet. From the results 16 of a bromide tracer test performed just before the start of the experiments, porosity (45% 17 and 28%) and pore volume (0.77 L and 0.52 L) were estimated for the CCC and the PTC 18 experiments, respectively. The columns were filled with water leaving a 4.5 cm free 19 nappe over the sediment to prevent the occurrence of a preferential flow pathway. Both 20 columns operated in downflow mode and the flow rate was controlled by a peristaltic 21 pump (Micropump Reglo Digital 4 channels ISMATEC). In both experiments, two stages 22 were defined separated by a lag period with no flow during which the columns were dried 23 and kept in the glove box. This lag period was used to simulate a dry period in an artificial 24 recharge set-up. During both stages (I and II), flow rate varied from 0.2 mL min<sup>-1</sup> to 0.4 25 mL min<sup>-1</sup>. The duration and flow rates of each stage are detailed later in this paper for 26 the CCC and PTC experiments, respectively. The input water was spiked with a NaNO<sub>3</sub> 27 solution to achieve a known nitrate concentration of between 0.8 mM and 2.9 mM for the 28 CCC experiment and between 0.7 mM and 3.5 mM for the PTC experiment.

Both flow-through experiments lasted over 7 months and 76 and 56 samples were
 collected from the outlet of the CCC and PTC, respectively.

### 3 2.2. Analytical methods

Anion (NO<sub>3<sup>-</sup></sub>, NO<sub>2<sup>-</sup></sub>, Cl<sup>-</sup> and SO<sub>4<sup>2-</sup></sub>) concentrations and isotope ratios ( $\delta^{15}N$  and  $\delta^{18}O$  of 4 5 dissolved NO<sub>3</sub><sup>-</sup>) were measured in all the batch experiment samples. In the flow-through 6 experiments, anions, cations,  $NH_4^+$ , non-purgeable dissolved organic carbon (NPDOC) 7 and dissolved inorganic carbon (DIC) were measured, and isotopic data were 8 determined for a subset of samples considered representative according to the 9 measured concentration of the target analyses. Redox potential (Eh) and pH were 10 measured daily at the column outflow with portable electrodes (WTW-3310). Aliquots of aqueous samples were filtered through 0.2 µm Millipore<sup>®</sup> filters. Anion concentration was 11 12 determined by high performance liquid chromatography (HPLC) with a WATERS 515 HPLC pump, IC-PAC anion columns and a WATERS 432 detector. For maior cation 13 14 analysis, samples were acidified with 1% HNO<sub>3</sub>. Cation concentrations were determined 15 by inductively coupled plasma-optical emission spectrometry (ICP-OES, Perkin-Elmer 16 Optima 3200 RL). NH₄<sup>+</sup> was analysed using ionic chromatography (DIONEX, ICS5000). 17 NPDOC was measured by organic matter combustion using a MULTI N/C 3100 Analytik 18 Jena carbon analyser. Periodically, 25 mL of aqueous solution was sampled to measure 19 dissolved inorganic carbon (DIC) by titration (METROHM 702 SM Titrino). Chemical 20 analyses were conducted at the the "Centres Científics i Tecnològics" of the Universitat 21 de Barcelona (CCiT-UB).

Stable isotopes are usually measured as the ratio between the heavier isotope (e.g.<sup>15</sup>N) and the lighter isotope (e.g.<sup>14</sup>N). These ratios are referenced to international standards using delta notation ( $\delta$ ), which is used to express the small variations in isotopic composition that occur and is defined by Eq. 4, where R=<sup>15</sup>N/<sup>14</sup>N.

26 
$$\delta^{15} N = \left[ \frac{(R_{sample} - R_{std})}{R_{std}} \right] \times 1000$$
 (Eq.4)

The isotopic analyses included the  $\delta^{15}N$  and  $\delta^{18}O$  of  $NO_3^-$ ,  $\delta^{15}N$  of  $NH_4^+$ ,  $\delta^{34}S$  and  $\delta^{18}O$ 1 2 of SO<sub>4</sub><sup>2-</sup>. The  $\delta^{15}$ N and  $\delta^{18}$ O of dissolved NO<sub>3</sub><sup>-</sup> were determined using a modified 3 cadmium reduction method (McIlvin and Altabet, 2005; Ryabenko et al., 2009). Briefly, 4  $NO_3^{-1}$  was converted to  $NO_2^{-1}$  through spongy cadmium reduction and then to nitrous oxide using sodium azide in an acetic acid buffer. Simultaneous  $\delta^{15}N$  and  $\delta^{18}O$  analysis of the 5 N<sub>2</sub>O produced was carried out using a Pre-Con (Thermo Scientific) coupled to a Finnigan 6 7 MAT-253 Isotope Ratio Mass Spectrometer (IRMS, Thermo Scientific). The δ<sup>15</sup>N of NH<sub>4</sub><sup>+</sup> 8 was analysed by the  $NH_4^+$  diffusion method using a Carlo Erba Elemental Analyser (EA) 9 coupled in a continuous flow to a Finnigan Delta C IRMS (Thermo Scientific). For  $\delta^{34}$ S and  $\delta^{18}$ O analyses, dissolved SO<sub>4</sub><sup>2-</sup> was precipitated as BaSO<sub>4</sub> by adding BaCl<sub>2</sub>·2H<sub>2</sub>O 10 11 after acidifying the sample with HCI and boiling it to prevent BaCO<sub>3</sub> precipitation, 12 following standard methods (Dogramaci et al., 2001). The  $\delta^{34}$ S was also analysed with the Carlo Erba EA -Finnigan Delta C IRMS. The δ<sup>18</sup>O was analysed in duplicate using a 13 ThermoQuest high temperature conversion elemental analyser (TC/EA) coupled in 14 15 continuous flow with a Finnigan MAT Delta C IRMS. For  $\delta^{13}C_{DIC}$ , carbonates were 16 converted to CO<sub>2</sub> gas by adding a phosphoric acid solution and the isotope ratio was 17 measured in a Gas-Bench II coupled to a MAT-253 IRMS (Thermo Scientific). The  $\delta^{13}$ C 18 and  $\delta^{15}N$ , as well as total C (%), of the two tested organic substrates were measured 19 using the Carbo Erba EA-Finnigan Delta C IRMS. Isotope ratios were calculated using 20 both international and internal laboratory standards. Notation was expressed in terms of 21  $\delta$  relative to the international standards (V-SMOW for  $\delta^{18}$ O, atmospheric N<sub>2</sub> for  $\delta^{15}$ N and V-CDT for  $\delta^{34}$ S). The reproducibility of the samples was ±1‰ for the  $\delta^{15}$ N of NO<sub>3</sub><sup>-</sup>, ±0.5‰ 22 for the  $\delta^{15}$ N of NH<sub>4</sub><sup>+</sup>, ±1.5‰ for the  $\delta^{18}$ O of NO<sub>3</sub><sup>-</sup>, ±0.2‰ for the  $\delta^{34}$ S of SO<sub>4</sub><sup>2-</sup> and ±0.5‰ 23 24 for the  $\delta^{18}O$  of SO<sub>4</sub><sup>2</sup>. Samples for isotopic analyses were prepared at the "Mineralogia Aplicada I Geoquímica de Fluids" laboratory and determined at the "Centres Científics i 25 26 Tecnològics" of the Universitat de Barcelona (CCiT-UB).

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### 1 **2.3. Isotope data evaluation**

Isotopic fractionation during denitrification can be expressed as a Rayleigh distillation
process (Eq. 5), from which the isotopic fractionation factor α can be obtained (Mariotti
et al., 1988; Aravena and Robertson, 1998).

$$Ln \left( \frac{R_t}{R_0} \right) = (\alpha - 1) * Ln \left( \frac{C_t}{C_0} \right)$$
(Eq.5)

6 where  $C_0$  and  $C_t$  are the initial and residual NO<sub>3</sub><sup>-</sup> concentrations, respectively (mmol L<sup>-1</sup>), 7 and R<sub>0</sub> and R<sub>t</sub> denote the ratios of heavy versus light isotopes in the initial and residual 8 isotopic ratios, respectively, which are calculated according to Eq. 6.

9 
$$R = \left[ \left( \frac{\delta}{1000} \right) + 1 \right]$$
 (Eq.6)

10 where  $\delta$  is the isotopic composition of  $\delta^{15}N$  and  $\delta^{18}O$  (‰). The term ( $\alpha$  - 1) was calculated 11 from the slope of the regression analysis in double-logarithmic plots [ln(R<sub>t</sub>/R<sub>0</sub>)] over 12 [ln(C<sub>t</sub>/C<sub>0</sub>)] according to Eq. 5, and converted to isotopic fractionation ( $\epsilon_N$  and  $\epsilon_O$ ) 13 according to Eq. 7.

14 
$$\varepsilon = 1000 \times (\alpha - 1)$$
 (Eq.7)

15 The Rayleigh equation applies to closed system conditions; therefore, isotopic 16 fractionation is commonly calculated in laboratory experiments where conditions are well 17 constrained, no other sinks affect the  $NO_3^-$  pool and the concentration and isotopic 18 composition of  $NO_3^-$  can be considered exclusively determined by  $NO_3^-$  reduction.

### 19 **3. Results**

Results of the batch experiments are detailed in supplementary material Table S1, and
results of the flow through experiments are detailed in Tables S2-S5.

### 22 **3.1. Batch experiments: chemical data**

In the sterilised control (SCB) and absence control (ACB) experiments,  $NO_3^-$  reduction did not occur. Results for CCB experiments showed complete  $NO_3^-$  consumption in less than 12 days (Fig. 1a). At t=0 (right after the groundwater spiked with NaNO3 was put in contact with the commercial compost) an initial NO3- release by the compost of up to 1 2.58 mM was observed. In the palm tree batch experiment (PTB), complete  $NO_3^{-1}$ 2 reduction was achieved in less than 20 hours with no significant initial  $NO_3$  release (Fig. 3 1b). In both batch experiments, transient NO<sub>2</sub><sup>-</sup> accumulation was observed. In the CCB 4 experiment, up to 0.1 mM of NO<sub>2</sub><sup>-</sup> was released on the first day, and thereafter NO<sub>2</sub><sup>-</sup> 5 concentration gradually decreased. In the PTB experiment, NO<sub>2</sub> transient accumulation 6 was more significant, with a concentration peak of 0.7 mM after 14 hours, which 7 corresponds to 81% of the initial NO<sub>3</sub> concentration. NO<sub>2</sub> content was negligible after 22 8 hours.

9

### 10 **3.2.** Flow-through experiments: chemical data

11 Results for the evolution of NO<sub>3</sub><sup>-</sup>, NO<sub>2</sub><sup>-</sup>, NH<sub>4</sub><sup>+,</sup> SO<sub>4</sub><sup>2-</sup>, NPDOC and DIC during the flow-12 through experiments are shown in Figures 2 (CCC) and 3 (PTC). The CCC experiment 13 was characterised by a large initial NO<sub>3</sub><sup>-</sup> release (up to 4.3 mM) in the first 4 days of 14 stage I. This NO<sub>3</sub> was released due to leaching from the compost, similarly to what was 15 observed in the CCB experiment. After that, complete NO<sub>3</sub><sup>-</sup> consumption was achieved. The decrease in  $NO_3^{-1}$  concentration was coupled with a slight increase in  $NO_2^{-1}$ , which 16 17 reached values of up to 1.3 mM in the first 7 days. A slight NH4<sup>+</sup> concentration was 18 detected in the output (values between 0.03 µM and 0.4 mM, Fig. 4a). The SO42-19 concentration in the input water was 1.9 mM, and in the outflow water it ranged from 0.4 mM to 3.8 mM. For most of stage I, outflow SO<sub>4</sub><sup>2-</sup> concentrations were below inflow 20 21 concentrations (Fig. 2). The concentration of NPDOC showed a sharp increase up to 22 38.4 mM during the first 4 days, followed by a rapid decrease to 0.1 mM (Fig. 2). DIC 23 content in the output samples was higher than in the inflow water throughout the 24 experiment, ranging from 6.8 mM to 8.9 mM (Fig. 2).

After the 7 week lag period, no NO3- leaching from the compost was observed and NO3concentrations decreased progressively to values below the detection limit (0.002mM). During this stage, no significant  $NO_2^-$  accumulation was observed. The outflow concentration values for  $NH_4^+$  and NPDOC in stage II remained close to the detection

limit (0.03 μM and 8 μM), and SO<sub>4</sub><sup>2-</sup>concentrations were below inflow concentrations by
 the end of this stage (after 213 days).

3 In the PTC experiment, no significant initial  $NO_3^{-1}$  and  $NO_2^{-1}$  release was observed (Fig. 3). 4 In contrast to the CCC experiment, a sharp increase in NH<sub>4</sub><sup>+</sup> (up to 6.3 mM after 1 day) 5 was detected (Fig. 4b). Similarly to the CCC experiment, outflow SO<sub>4</sub><sup>2-</sup> concentrations 6 were below inflow concentrations for most of stage I. NPDOC concentrations remained 7 stable at between 0.1 mM and 0.2 mM and, in contrast to the CCC experiment, there 8 was no sharp increase at the beginning of the experiment (Fig. 3). Output DIC values 9 were lower than input values except on the first day (Fig. 3). After the lag period, 10 complete denitrification was again achieved, although small  $NO_3^{-}$  peaks were observed, 11 probably due to flow rate changes. Similarly to the CCC experiment, no significant  $NO_2^{-1}$ 12 or NH4<sup>+</sup> accumulation was observed and outflow sulphate concentrations were below 13 inflow concentrations by the end of stage II (after 173 days). The main difference was a 14 significant initial NPDOC release (up to 2.5 mM).

15

### 16 **3.3. Isotopic results**

In the CCB experiment, an increase of both  $\delta^{15}$ N-NO<sub>3</sub><sup>-</sup> (from +9.4‰ to +65.6‰) and  $\delta^{18}$ O-17 18  $NO_3^-$  (from +18.6‰ to +52.6‰) was observed as the  $NO_3^-$  concentration decreased 19 (Supplementary material, Table S1). In the PTB experiment, the  $\delta^{15}N$  of dissolved NO<sub>3</sub><sup>-</sup> 20 increased (from +15.40% to +32.10%) as the NO<sub>3</sub><sup>-</sup> concentration decreased (Table S1). 21 In the latter experiment, rapid NO3<sup>-</sup> consumption promoted considerable NO2<sup>-</sup> accumulation, hindering the determination of  $\delta^{18}O_{NO3}$ . A subset of 22 outflow samples 22 23 from the CCC experiment and 14 samples from the PTC experiment was selected for 24  $NO_3^{-}$  and  $NH_4^{+}$  isotopic analyses. In the CCC experiment, the isotopic composition of dissolved NO<sub>3</sub><sup>-</sup> showed an increase from +15.0% to +61.3% for  $\delta^{15}$ N, and from +10.6% 25 to +52.2‰ for  $\delta^{18}$ O during the first 10 days of stage I, coinciding with the complete 26 consumption of NO<sub>3</sub><sup>-</sup> (Supplementary material, Table S3) . In stage II,  $\delta^{15}$ N and  $\delta^{18}$ O 27 28 increased during the two periods of  $NO_3^-$  reduction (up to +60.7‰ and +49.8‰,

1 respectively) (Table S3) separated by a NO<sub>3</sub><sup>-</sup> rebound linked to an increase in flow rate 2 up to 0.4 mL min<sup>-1</sup> (from 154 to 165 days). Stage II of the PTC experiment showed a 3 similar trend to that of the CCC experiment, whereby the isotopic composition of 4 dissolved NO<sub>3</sub><sup>-</sup> showed an increase from +16.5‰ to +53.2‰ for  $\delta^{15}$ N, and from +21.4‰ 5 to +62.3‰ for  $\delta^{18}$ O, coinciding with the complete consumption of NO<sub>3</sub><sup>-</sup> (Supplementary 6 material, Table S5). The  $\delta^{15}$ N values of dissolved NH<sub>4</sub><sup>+</sup> ranged between +7.1‰ and 7 +11.4‰ in the CCC experiment, whereas a wider range of values was observed in the 8 PTC experiment, from +2.2‰ to +17.9‰ (Fig. 4).

9 The  $\delta^{13}C_{DIC}$  was determined in a subset of 28 samples from stage I of the CCC experiment and 15 samples from both stages of the PTC experiment. The  $\delta^{13}C_{DIC}$  values 10 11 ranged from -13.2‰ to -18.6‰ for the CCC experiment and from -10.3‰ to -18.0‰ 12 (stage I) and from -16.0% to -16.9% (stage II) for the PTC experiment. A subset of 25 samples from each experiment, with varying SO<sub>4</sub><sup>2</sup> concentrations, was analysed to 13 determine the isotopic composition of dissolved SO<sub>4</sub><sup>2-</sup> ( $\delta^{34}$ S<sub>SO4</sub> and  $\delta^{18}$ O<sub>SO4</sub>). In the CCC 14 experiment, the outflow  $\delta^{34}$ S and  $\delta^{18}$ O values ranged from +7.7‰ to +22.4‰ and from 15 16 +10.1‰ to +13.6‰, respectively (Supplementary material, Table S3). In the PTC experiment, values ranged from +9.1% to +10.6% for  $\delta^{34}$ S, and from +11.2% to +11.1% 17 18 for  $\delta^{18}O$  (Supplementary material, Table S5)

19

### 20 4. Discussion

### 4.1. Nitrogen - sulphate geochemistry and nitrate attenuation

Complete  $NO_3^-$  attenuation was achieved in all the experiments. In the column experiments, the CCC experiment showed an initial  $NO_3^-$  release, a temporary  $NO_2^$ accumulation, and a slight  $NH_4^+$  increase, whereas in the PTC experiment very low  $NO_2^$ accumulation and a large initial  $NH_4^+$  increase was observed. This increase in  $NH_4^+$  might indicate  $NH_4^+$  leaching from vegetal decomposition, but could also be generated by DNRA. If  $NH_4^+$  was leached from the organic substrates, its isotopic composition should

1 be in agreement with the reactive material (compost/palm leaves). This was observed in 2 the CCC experiment and in the first days of the PTC experiment (Fig. 4). Therefore, it is 3 reasonable to assume that  $NH_4^+$  leaching was the main source of  $NH_4^+$  observed at the 4 beginning of both experiments. However, by the end of stage I of the PTC experiment, 5  $\delta^{15}N_{NH4}$  values were significantly higher (up to +16.2‰), a finding that could not be 6 explained by leaching. Instead, a feasible hypothesis is the occurrence of DNRA. In 7 general terms, DNRA is favoured under higher C to  $NO_3^{-1}$  ratios when the electron 8 acceptor (NO<sub>3</sub>) becomes limiting and the system is rich in labile carbon (Korom et al., 9 1992; Burgin and Hamilton, 2007). Accordingly, the highest C/N ratio was observed in 10 the stage I of the PTC experiment when  $NH_4^+$  isotope data discards  $NH_4^+$  leaching and 11 points to the occurrence of DNRA. Nevertheless, DNRA can also occur under low C/N 12 ratios (Carrey et al., 2014). In addition, it seems that the type of organic carbon may have 13 some role in the development of denitrification or DNRA. Further research is needed to 14 better understand which process is taking place. However, the extent of DNRA in the 15 present experiments was limited, since even assuming that NH4<sup>+</sup> was derived from 16 DNRA, this would only account for a maximum of 15% of NO<sub>3</sub><sup>-</sup> attenuation in the PTC 17 experiment. Therefore, the main  $NO_{3}$  attenuation process in both experiments was 18 denitrification.

19 The NO<sub>3</sub> reduction pathway depends on the biomass present in the system, which is 20 controlled by the type of organic carbon available (Nijburg et al., 1998). In addition, Abell 21 et al. (2009) have reported that DNRA bacteria have the capacity to use organic 22 substrates unavailable to denitrifier bacteria. It is reasonable to assume that the 23 differences observed in the two experiments with regard to NH<sub>4</sub><sup>+</sup> generation could be 24 explained by the different organic matter used as electron donor. Palm tree leaves have 25 the capacity to release more NH4<sup>+</sup> than commercial compost, besides being a labile 26 organic substrate that facilitates  $NH_4^+$  formation through the DNRA process. These 27 results are consistent with the marked differences in NPDOC values obtained in the first sample of the batch experiments: 150 mg L<sup>-1</sup> for the PTB and 4 mg L<sup>-1</sup> for the CCB. 28

After the lag period, in stage II of both experiments a faster denitrification was observed. Therefore, it was demonstrated a high denitrification potential for these two types of organic material (CC and PT). These substrates might be used in ARP, where the conditions are variable; even during dry periods, when a potential entry of oxygen might occur.

SO<sub>4</sub><sup>2-</sup> reduction may be promoted when NO<sub>3</sub><sup>-</sup>, Mn and Fe have been entirely consumed 6 7 but organic carbon is still available. The input water contained Fe and Mn concentrations 8 below the detection limit (2  $\mu$ M and 0.2  $\mu$ M, respectively); therefore, once the NO<sub>3</sub><sup>-</sup> had 9 been completely consumed,  $SO_4^{2-}$  reduction could occur according to the redox 10 sequence in natural systems, since most of the organic matter was still available for 11 degradation. For most of stage I and by the end of stage II in both the CCC and PTC 12 experiments, SO<sub>4</sub><sup>2-</sup> consumption was observed once all the NO<sub>3</sub><sup>-</sup> had been removed. In 13 addition, in both experiments, Eh was close to the values that have been reported to promote SO<sub>4<sup>2-</sup></sub> reduction (below -150 mV, Connell and Patrick, 1968). Isotope results 14 15 confirmed the occurrence of sulphate reduction (see Supporting material).

16

### 17 **4.2.** Denitrification rate and organic C reactivity

18 In order to quantitatively compare the reactivity of the two organic carbon sources, we 19 developed a kinetic model of the two batch experiments. As the observed NO<sub>2</sub>-20 concentration in the experiments was high (up to 33.4 mg L<sup>-1</sup>), the model considered two 21 main processes: 1) the degradation of  $NO_3$  into  $NO_2$ , and 2) the degradation of  $NO_2$ 22 into  $N_2(q)$ . We tested different kinetics during the modelling process, and found that the 23 best combination was zero order kinetics for the degradation of  $NO_3^-$  into  $NO_2^-$  (Eq. 8) 24 and first order degradation considering inhibition by  $NO_3$  for the degradation of  $NO_2$  into 25  $N_2(g)$  (Eq. 9).

26 
$$r_{NO_3^-} = -K_1$$
 (Eq.8)

27 
$$r_{NO_2^-} = +QK_1 - K_2[NO_2^-] {K_i / K_i + [NO_3^-]}$$
 (Eq.9)

1 where r is the degradation rate of  $NO_3^-$  and  $NO_2^-$  [ML<sup>-3</sup>T<sup>-1</sup>], K<sub>1</sub> is the zero degradation 2 constant [ML<sup>-3</sup>T<sup>-1</sup>], Q is the stoichiometric ratio between NO<sub>3</sub><sup>-</sup> and NO<sub>2</sub><sup>-</sup> (1) [-], K<sub>2</sub> is the 3 first order degradation rate [T<sup>-1</sup>], and K<sub>i</sub> is the inhibition parameter [ML<sup>-3</sup>]. These results 4 contrast with those reported in previous studies, where the model that fit best was the 5 Monod kinetic model (e.g. Rodriguez-Escales et al., 2014; Carrey et al., 2014a). Zero 6 order kinetics is achieved when the substrate is not limiting. In this case, we supposed 7 that organic carbon was not limiting. Note that the amount of organic carbon in the 8 system was much higher than the amount of NO3- (Table 1 and 3). However, the 9 degradation of NO<sub>2</sub><sup>-</sup> into N<sub>2</sub>(g) was limited by the presence of NO<sub>2</sub><sup>-</sup> (first order kinetics 10 with respect to  $NO_2$ ). Both rates were solved numerically considering a time step of 0.5 11 d in the CCB experiment and 0.01 d in the case of PTB. Figure 5 gives the results of the 12 model considering the parameters listed in Table 3 and an initial concentration of  $NO_3$ 13 of 2.49 mM for CCB and 0.86 mM for PTB. The initial concentrations were based on the 14 initial measurements of the NO<sub>3<sup>-</sup></sub> in the batch experiments (see Table S1). Note that the 15 initial NO3<sup>-</sup> concentration in the CCB experiment was higher due to the fast leaching of 16  $NO_3^{-}$  from the compost. Regarding the parameters, it can be observed that the K<sub>1</sub> value 17 was 10 times higher in the PTB experiment than in the CCB experiment (Table 3), 18 resulting in a characteristic time (i.e. the inverse of the reaction rate constant) of 0.5 days 19 for PTB compared to 3.7 days for CCB. As NO<sub>2</sub> production in the PTB experiment was 20 much faster than in the CCB one, and NO<sub>2</sub> degradation rates were relatively similar in 21 both experiments, higher NO<sub>2</sub> accumulation was expected in the PTB experiment (Fig. 22 5). Kinetic analysis of the column experiments was based on a N input-output mass 23 balance. The  $NO_3^-$  concentration in the inflow water (plus  $NO_3^-$  nitrate initially leached 24 from the compost and NH<sub>4</sub><sup>+</sup> initially leached from the palm tree leaves) was considered 25 as the input of the system, while outflow concentrations of NO3, NO2 and NH4<sup>+</sup> were 26 considered as the output. Any gaseous species such as  $N_2O$  or  $N_2$  were not considered 27 because they were not measured. The percentage of N consumption was calculated for 28 each stage of both column experiments as the difference between the input and the output N masses in the system (Supplementary material, Table S6). During stage I,
higher N consumption was achieved with the palm tree leaves than with the compost,
although similar N consumption percentages were obtained in both cases after the lag
period.

5 Total NO<sub>3</sub><sup>-</sup> removed during the experiments was 83.7 mmol for the CCC experiment and 6 139.7 mmol for the PTC experiment, respectively (Table S6). The stoichiometric amount 7 of C needed for the observed NO<sub>3</sub><sup>-</sup> and SO<sub>4</sub><sup>2-</sup> depletion were calculated according to the 8 denitrification reaction (Eq.2), the DNRA reaction (Eq.10) and the sulphate reduction 9 reaction (Eq.11), respectively.

$$(NO_3^- + 2CH_2O + 2H^+ \to NH_4^+ + 2CO_2 + H_2O)$$
 (Eq. 10)

11

12

 $(SO_4^{2-} + 2CH_2O + H^+ \to HS^- + 2CO_2 + 2H_2O)$ (Eq.11)

Obtained values (125.3 mmols C for CCC and 194.8 mmols C for PTC) corresponded to 0.8% and 3.7% of the total C in both substrates. Degradable organic C, including the organic carbon leached from the substrates, corresponded to 2.4% and 4.2% of the total C present in the commercial compost and palm tree leaves, respectively. Similar reactive organic C percentages have been obtained in other column experiments using fresh or old organic matter (between 2% and 6%, Abell et al., 2009; Carrey et al., 2013).

Palm tree leaves gave a higher denitrification yield (i.e. amount of  $NO_3$  nitrate consumed per amount of available C) than CC (6 versus 33 mmol  $NO_3$  / mol  $C_{org}$ ), probably because the organic carbon was easily degradable by the bacteria present in the water, enabling them to grow rapidly and produce complete  $NO_3$  attenuation in a short period of time.

23 **4.3**.

### 8. Nitrate isotope fractionation

In the CCB and CCC experiments, denitrification was the only process consuming NO<sub>3</sub><sup>-</sup> . In order to calculate the  $\varepsilon_N$  and  $\varepsilon_O$  values, all the samples from both batch and column experiments were plotted together due to the similar trends observed. Figure 6 shows the Rayleigh model for CCC and CCB. Using Eq. 9, isotopic fractionations were calculated as -10.8‰ for  $\varepsilon_N$  and -9.0‰ for  $\varepsilon_O$ , with a  $\varepsilon_N/\varepsilon_O$  of 1.2. Due to the fast rate of NO<sub>3</sub><sup>-</sup> consumption and the transient NO<sub>2</sub><sup>-</sup> accumulation in the experiments with palm tree leaves, it was not possible to calculate isotopic fractionation in the batch experiments: calculations were therefore based only on the PTC experiment. Furthermore, as DNRA was detected, the isotopic fractionation obtained was an estimation of the isotope ratio changes for both competing processes. The values obtained were  $\varepsilon_N$ = -9.9‰ and  $\varepsilon_O$ = - 8.6‰ with a  $\varepsilon_N/\varepsilon_O$  of 1.15 (Figure 6).

8 The  $\varepsilon_N$  and  $\varepsilon_O$  values obtained were almost equal when using compost or palm tree 9 leaves as substrates, despite the different NO<sub>3</sub><sup>-</sup> reduction rate and the limited contribution 10 of DNRA in the PTC. With high denitrification rates, some authors have observed lower 11 isotopic fractionation (Mariotti et al., 1988) whereas others have reported higher 12 fractionation (Korom et al., 2012). In the present study, isotopic fractionation did not show 13 any effect related to changes in the attenuation rate, in agreement with previous 14 laboratory experiments (Carrey et al., 2014b). An overview of isotopic fractionation 15 estimated from several laboratory studies is presented in Table 4.

16 The  $\varepsilon_N$  and  $\varepsilon_O$  values obtained in the present study fell within the range of values reported 17 in the literature. The  $\varepsilon_N$  values obtained were at the lower end of induced denitrification 18 experiment values (Knöller et al., 2011; Carrey et al., 2014b). In general, autotrophic 19 denitrification or pure culture experiments have obtained higher  $\varepsilon_N$  values (in absolute 20 terms) (Table 4). With regard to  $\varepsilon_0$ , some authors have reported an inverse fractionation 21  $(\epsilon_0 > 0\%)$  due to <sup>16</sup>O loss during reduction of NO<sub>3</sub><sup>-</sup> to N<sub>2</sub>O (Casciotti et al., 2002; Toyoda 22 et al., 2005). The  $\varepsilon_0$  calculated in the present study showed normal fractionation within 23 the range of reported values for heterotrophic denitrification.

Recent studies have focused on the  $\varepsilon_N/\varepsilon_0$  ratio in order to elucidate different processes affecting isotopic fractionation during NO<sub>3</sub><sup>-</sup> reduction (Granger et al., 2008; Knöller et al., 2011). Factors such as pH, salinity or carbon sources have been reported to show no effect on the  $\varepsilon_N/\varepsilon_0$  ratio (Granger et al., 2008; Wunderlich et al., 2012). The incorporation of oxygen isotopes from water into NO<sub>3</sub><sup>-</sup> and NO<sub>2</sub><sup>-</sup> and re-oxidation of NO<sub>2</sub><sup>-</sup> to NO<sub>3</sub><sup>-</sup> have

1 been observed to modify  $\varepsilon_0$  in field studies. These processes tend to reduce  $\varepsilon_0$  values, 2 increasing the  $\varepsilon_N/\varepsilon_0$  ratio up to 1.8 - 2.0. In denitrification laboratory experiments, a wider 3 range has been observed, from 0.96 (Carrey et al., 2013) to 2.9 (Knöller et al., 2011). 4 Higher values can be achieved when important  $NO_2^-$  accumulation and  $NO_2^-$  re-oxidation 5 is produced (Knöller et al., 2011). The  $\varepsilon_N/\varepsilon_O$  ratios obtained in the present experiments 6 were of 1.12 for CCB-CCC and 1.15 for PTC. As palm and compost experiments were 7 performed under anaerobic conditions and  $NO_2^-$  accumulation only lasted for a few days, 8 re-oxidation of NO<sub>2</sub><sup>-</sup> can be ruled out. In addition, due to rapid NO<sub>3</sub><sup>-</sup> reduction and the 9 high isotopic composition of  $\delta^{18}O_{NO3}$  (up to +62.3‰), the equilibrium isotope fractionation 10 between water and  $NO_3^{-}$  can be considered negligible compared to kinetic isotope 11 fractionation during  $NO_3$  reduction.

12 Composition of the microbial community can also affect the  $\epsilon_N/\epsilon_O$  ratio during 13 denitrification (Dähnke and Thamdrup, 2016). Deviations in  $\varepsilon_N/\varepsilon_O$  ratios can be produced 14 by different enzymes involved in  $NO_3^-$  reduction (Granger et al., 2008). Activity of the 15 periplasmic NO<sub>3<sup>-</sup></sub> reductase (Nap) in denitrifying bacteria resulted in a  $\varepsilon_N/\varepsilon_0$  value of ~1.6 16 (Granger et al., 2008). However, membrane-bound respiratory  $NO_3$  reductase (Nar) is 17 more common in classical heterotrophic denitrification and tends to produce  $\epsilon_N/\epsilon_O$  values 18 of ~1.0 (Granger et al., 2008). The  $\varepsilon_N/\varepsilon_0$  ratios obtained in the present experiments were 19 close to 1.0, suggesting a lower influence of periplasmic  $NO_3^-$  reductase, in agreement 20 with NO<sub>3</sub> reduction driven by heterotrophic denitrification. As some DNRA was observed 21 in the palm experiment, a higher  $\epsilon_N/\epsilon_0$  would be expected, since the reduction of NO<sub>3</sub> to 22  $NO_2$  by DNRA is considered to be mainly catalysed by Nap complex (Kraft et al., 2011). 23 However, the  $\varepsilon_N/\varepsilon_O$  observed in PTC was 1.15, similar to compost (1.12), in agreement 24 with the main role of heterotrophic denitrification in NO<sub>3</sub><sup>-</sup> attenuation. Likewise, the  $\epsilon_N/\epsilon_0$ 25 ratio in both experiments was close to values obtained in other laboratory experiments 26 involving induced or natural denitrification in freshwater (Granger et al., 2008; Carrey et 27 al., 2013; Carrey et al., 2014b). The published results suggest that denitrification 28 produces ratios of around 1.0 and any deviation can be related to equilibrium isotope

1 fractionation, re-oxidation of  $NO_2^-$  or a different biological pathway of  $NO_3^-$  reduction.

Induced denitrification at field scale may be masked by several processes, such as dispersion, diffusion or dilution (mixing) that could change the NO<sub>3</sub><sup>-</sup> concentration in groundwater. The isotopic fractionation of N and O for dissolved NO<sub>3</sub><sup>-</sup> obtained in labscale experiments may be used in future studies to assess system behaviour in the field and optimise full-scale application.

### 7 5. Conclusions

This study shows that CC and PT have a satisfactory capacity to promote complete denitrification, even after a lag stage without flow, simulating a dry period. However, a potential drawback in the use of these substrates is the initial NH<sub>4</sub><sup>+</sup> release and the slight NO<sub>2</sub><sup>-</sup> accumulation observed suggesting the necessity of a pre-treatment of the material previously to be installed in the MAR system. Overall, the PT gave higher denitrification rate and yield making it suitable for MAR systems in arid and semi-arid climates, where short-term efficient organic substrate is required.

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### 9 Figure captions

Figure 1. Variation in NO<sub>3</sub><sup>-</sup> and NO<sub>2</sub><sup>-</sup> concentrations over time in the batch experiments.
(a) CCB and ACB experiments. (b) PTB and SCB experiments. Values and error bars
represent the mean and standard deviation, respectively, for the three replicate
experiments. Input-NO<sub>3</sub><sup>-</sup> concentration is also shown.

Figure 2. Changes in NO<sub>3</sub><sup>-</sup>, NO<sub>2</sub><sup>-</sup>, NH<sub>4</sub><sup>+</sup>, SO<sub>4</sub><sup>2-</sup>, DIC and NPDOC outflow concentrations
over time under variable operating conditions for the CCC experiment. NO<sub>3</sub><sup>-</sup>, SO<sub>4</sub><sup>2</sup> and
DIC content of the inflow water are also shown (continuous and dashed lines,
respectively). Content of NPDOC in the input water was low (0,1 mgL<sup>-1</sup>).

**Figure 3.** Changes in NO<sub>3</sub><sup>-</sup>, NO<sub>2</sub><sup>-</sup>, NH<sub>4</sub><sup>+</sup>, SO<sub>4</sub><sup>2-</sup>, DIC and NPDOC outflow concentrations over time under variable operating conditions for the PTC experiment. NO<sub>3</sub><sup>-</sup>, SO<sub>4</sub><sup>2-</sup> and DIC content of the inflow water are also shown (continuous and dashed lines, respectively). Content of NPDOC in the input water was low (0,1 mgL<sup>-1</sup>).

Figure 4. Changes in NH<sub>4</sub><sup>+</sup> concentration and isotopic composition over time in the outflow of both column experiments. (a) CCC and (b) PTC experiments. In both experiments, dashed lines represent the range of measured values of the  $\delta^{15}$ N for each material

- **Figure 5.** Results of the model for the (a) CCB experiment and the (b) PTB experiment.
- 2 Open symbols represent experiment results, whereas dashed and continuous lines
- 3 represent model results
- **Figure 6.** (a) and (c)  $\delta^{15}$ N and (b) and (d)  $\delta^{18}$ O of NO<sub>3</sub><sup>-</sup> against the natural logarithm of
- 5 the NO<sub>3</sub><sup>-</sup> concentration of CCB-CCC (upper panels) and PTC (lower panels). Slopes of
- 6 the regression lines represent ( $\alpha$ -1), the isotopic fractionation factor for N and O.

### 8 Table captions

- 9 Table 1. Summary of key parameters of both organic substrates used in the present
- 10 experiments: CC and PT
- **Table 2.** Experimental conditions of the batch experiments.
- **Table 3.** Kinetic parameters used for modelling batch experiments.
- 13 Table 4. Estimated isotopic enrichment factor (εN and εO) obtained in this study and
- 14 reported in the literature for in situ natural denitrification in laboratory experiments.











b





**Table 1.** Summary of key parameters of both organic substrates used in the presentexperiments: commercial compost (CC) and palm tree leaves (PT)

Organic substrate	N(%)	C <sub>total</sub> (%)	δ <sup>15</sup> N (‰)	δ <sup>13</sup> C (‰)
CC	1.0±0.2	15.1±1.1	12.1±1.1	-25.1±0.2
PT	1.5±0.6	47.4±0.9	3.6±0.8	-27.1±0.2

Code	Experiment	Contents of the incubation
CCB	Triplicate (1,2,3)	20 g commercial compost, 400 mL groundwater, 0.80 mM NO <sub>3</sub> -
SCB	Sterilized control	11 g autoclaved crushed palm leaves, 400 mL sterilized groundwater, 0.80 mM NO <sub>3</sub> -
РТВ	Triplicate (1,2,3)	11 g palm leaves, 400 mL groundwater, 0.80 mM $NO_3^-$
ACB	Absence control	400 mL groundwater, 0.80 mM NO <sub>3</sub> -

**Table 2.** Experimental conditions of the commercial compost (CCB), sterilized control (SCB),palm tree leaves (PTB) and absence control (ACB) batch experiments

 Table 3. Kinetic parameters used for modelling batch experiments

Experiment	NO <sub>3</sub> - to NO <sub>2</sub> -	$NO_2^-$ to $N_{2(g)}$	
Experiment	K₁ (mM d⁻¹)	K₂ (d⁻¹)	K <sub>i</sub> (mM)
ССВ	0.27	9	0.8
РТВ	2	6.5	0.01

	εN (‰)	εO (‰)	εΝ/εΟ	Reference	Commnets	
Heterotrophic denitrification						
Pure cultures	-20 to -30	n.d.	n.d.	Wellman et al. (1968)	Batch, Penassay Broth medium, Psedumonas stutzeri	
	-13.4 to -20.8	n.d.	n.d.	Delwiche and Steyn (1970)	Batch, glucose, Pseudomonas denitrificans	
	-28.6	n.d.	n.d.	Barford et al. (1999)	Steady-state reactor, acetate, Paracoccus denitrificans	
	-39 to -31	+13 to +32	n.d.	Toyoda et al. (2005)	Batch, citrate, Pseudomonas fluorescens	
	-22 to -17	-3 to -1	n.d.	Toyoda et al. (2005)	Batch, citrate, Pseudomonas fluorescens	
	-22 to -10	+4 to +23	n.d.	Toyoda et al. (2005)	Batch, citrate, Paracoccus denitrificans	
	-12.7	n.d.	n.d.	Sutka et al. (2006)	Batch, citrate, Pseudomonas chlororaphis	
	-36.7	n.d.	n.d.	Sutka et al. (2006)	Batch, citrate, Pseudomonas chlororaphis	
	-18.1 and -17.3	-16.5 and -16.1	1.07 to 1.09*	Wunderlich et al. (2012)	Batch, toluene, Thauera aromatica and Aromatoleum aromaticum	
	-18.9	-15.9	1.19*	Wunderlich et al. (2012)	Batch, benzoate, Thauera aromatica	
	-22.1 and -23.5	-19.9 and -23.7	1.0 to 1.1*	Wunderlich et al. (2012)	Batch, acetate, Thauera aromatica and Aromatoleum aromaticum	
	-8.6 and -16.2	-4.0 and -7.3	1.26 to 2.94	Knöller et al. (2011)	Batch, succinate and toluene, Azoarcus sp. and Ps. pseudoalcaligenes	
Seawater	-5.4 to -26.6	-4.8 to -22.6	1.0 to 1.8	Granger et al. (2008)	Batch, seawater, pure cultures	
	-14.6	n.d.	n.d.	Grischek et al. (1998)	Column, sediment from sandy silty and gravel aquifer and river water	
Freshwater sediment	-32.9 to -34.1	n.d.	n.d.	Tsushima et al. (2006)	Column, aquifer sediment and groundwater	
	-11.6 and -15.7	-12.1 and -13.8	0.96 to 1.14	Carrey et al. (2013)	Column, organic- and sulfide-rich sediments and groundwater	
Freshwater sediment bioestimulated	-17.1	-15.1	1.1	Vidal-Gavilan et al. (2013)	Batch, aquifer material and groundwater + glucose	
	-13	-8.9	1.5	Vidal-Gavilan et al. (2013)	Batch, aquifer material and groundwater + ethanol	
	-6.5	-6	1.01	Vidal-Gavilan et al. (2014)	Column, aquifer material and groundwater + ethanol	
	-8.8	-8	1.1	Carrey et al. (2014)	Column, aquifer sediment and groundwater + glucose	
	-10.4	-9	1.3	This study	Column and batch, groundwater + commercial compost	
	-9.9	-8.6	1.15	This study	Column, groundwater + palm tree leaves	
Autotrophic denitrification						
	-15.0 and -22.9	-19.0 and -13.5	1.2	Torrentó et al. (2010)	Batch, pyrite, pure culture (Th. denitrificans)	
	-12.6	-8.8	1.43	Hosono et al. (2015)	Batch, pyrite, pure culture (Th. denitrificans)	
	-25.0 and -27.6	-13.5 and -21.3	1.3	Torrentó et al. (2011)	Batch, aquifer sediment + pyrite	

**Table 4.** Estimated isotopic enrichment factor (εN and εO) obtained in this study and reported in the literature for denitrification lab experiments.

n.d. = not dertermined, (\*) Values estimated from published data